*DE 19545701-C1 A(3-A4A, 8-D, 11-B5D, 11-C2, 12-W11A) J(1-C3)	own base membrane adding with aqueous a with disaldehyde good stability in organic solvents, which is produced by a simple, low-cost process without using organic solvents or environmentally harmful substances.	a known base) of cellulose embrane (A) is AC is crosslinked PREFERRED MEMBRANE The HAC is crosslinked with dialdehydes(s), preferably glyoxal and the common of the consists of polyether-imide, polyacrylonitrile, polysulphone or PVDF. Layer (B) has a thickness of 0.01-0.5 micron. The NFM has a		than 70° C are used for separation processes h mol. wts. of 200-
97-282334/26 A88 J01 GKSS FORSCHUNGSZENTRUM GEESTHACHT GMBH	95.12.07 95DE-1045701 (97.05.28) B01D 69/12, 61/00, 67/00 Composite nano-filtration membrane - has known base membrane and selective separation layer made by coating with aqueous hydroxyalkyl cellulose solution and crosslinking with di:aldehyde C97-090945 Addnl. Data: SCHMIDT M, PEINEMANN K	Composite nano-filtration membrane (NFM) with a known base membrane (A) and a selective separation layer (B) of cellulose hydroxyalkyl ether (HAC) is claimed, in which membrane (A) is coated with an aqueous solution of HAC and the HAC is crosslin with acetal groups by reaction with aldehyde(s).	Also claimed is a process for the production of NFM by coating (A) with an aqueous solution of HAC and crosslinking the HAC as above.	USE In membrane filtration processes for the separation of the components of systems containing substances with mol. wts. of 200-

wt. compounds in aqueous systems contaminated with 10 wt% organic values of 600, 610, 590, 575, 620 and 525 for mixtures contaminated with acetone, MEK, ethanol, isopropanol, THF and EtOAc (5 wt%) with glutaric dialdehyde for 20 mins, at 70° C. The membranes were membrane pressure difference of 10 bar, using solutions of low-mol. Under these conditions the membranes showed mol. wt. cut-off wt% aqueous hydroxypropyl-cellulose solution and then crosslinked respectively, with corresponding substance flow rates of 1.25, 1.32, Asymmetric polyether-imide membranes were coated with 0.1 then evaluated in dead-end filtration tests at 20° C with a trans-.22, 1.19, 1.46 and 1.11 I/m²/hr./bar. (SL) 6pp1712DwgNo.0/0) solvent.